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Improvement in Generation of Bio-Gas Assuming Food Waste as Additional Feed

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Abstract: Due to scarcity of petroleum and coal it threatens supply of fuel throughout the world also problem of their combustion led to research in different corners to get access the new sources of energy, like renewable energy resources. Solar energy, wind energy, different thermal and hydro sources of energy, biogas are all renewable energy resources. But, biogas is separate from supplementary renewable energies for the reason that of its individuality of by means of, controlling and collecting organic wastes and at the same time producing fertilizer and water for use in agricultural irrigation. Biogas does not have any geographical limitations nor does it require advanced technology for producing energy, also it is very simple to use and apply. Kitchen waste is organic material having the high calorific value and nutritive value to microbes, that's why efficiency of methane production can be increased by several order of magnitude as said earlier. It means higher efficiency and size of reactor and cost of biogas production is reduced.

I. INTRODUCTION

Deforestation is a very big problem in developing countries like India, most of the part depends on charcoal and fuel-wood for fuel supply which requires cutting of forest. Also, due to deforestation it leads to decrease the fertility of land by soil erosion. Use of animal dung, firewood as energy is also harmful for the health of the masses due to the smoke arising from them causing air pollution. We need an eco friendly substitute for energy. Now days in India an organic waste is a major issue as it is covering up to 40 % of total waste. The organic waste can be hazardous and led to environmental & health issues. Besides it we are generating huge waste but fact is we don't have much area for dumping. BIOGAS forms by microorganism through the bio-degradation of organic material in anaerobic conditions. Natural generation of biogas is a vital part of bio-chemical carbon cycle. It can be used both in rural and urban areas. Biogas is a clean and efficient fuel. It is a mixture of: – Methane (CH4) – Carbon dioxide (CO2) – Hydrogen (H2) – Hydrogen Sulphide (H2S). The chief constituent of biogas is methane (65%).

II. OBJECTIVES

- Overall design factor to compare with typical plants for Optimization of gas production considering effect of various parameters
- To achieve maximum production of methane to maintain temperature at 35° C of slurry supply as well digester for the proposed plant for Mp Nagar zone 1 Bhopal area.

- Calculation of thermal effect over production of biogas, observing convection and conduction factor.
- Total & volatile solid concentration
- Quantitative relation between Carbon and nitrogen

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PRIMARY PREPARATION COLLECTION OF KITCHEN WASTE:-

At primary stage for kitchen waste collection is to separate bio degradable waste among others, with identifying various color dust bean or bag.

It will help to separate kitchen waste as well reduce time consumption, and hence it will be easy to carry these to the prepared site. So that the aimed output for methane can be optimized as follows given in table:

| 1 | TABLE - 1 |
|-----------------|----------------------|
| ELEMENTS | VOLUME IN PERCENTAGE |
| METHANE | 55 - 65 |
| CARBON DI-OXIDE | 30-40 |
| NITROGEN | 03 - 07 |
| WATER VAPOUR | 0.5 - 1 |

Separation of material on primary basis according to capability to increase production rate of methane as follows:

| Table – 2 Biogas | s rate of producing r | nethane |
|----------------------|------------------------------|------------|
| Materials and their | Biogas in m ³ /kg | Methane |
| main components | TS | percentage |
| Leaves | 0.251-0.30 | 58 |
| Brewery liquid waste | .0300600 | 58 |
| Rice | 0.790 | 51 |
| Slurry | 1.45 | 72-75 |
| Protein | 0.100 | 50 |
| Animal dung | 0.280-0.285 | 55-60 |

Table – 2 Biogas rate of producing methane

According to BMC, roughly 50 % of the waste was of biodegradable nature, 15-20% comprised of polythene waste and rest was non-biodegradable waste. A study by Katiyar, Suresh, & Sharma in 2013 characterized waste in Bhopal as follows. Approximately 40-45 % of the waste was food and FVW and 10% was inert waste such as dust, sand, soil etc. Metals comprised about 1% of the waste. The study indicated that Bhopal had mixed residue (organic matter mixed with soil, mud and other inert matter) to the extent of 81%. Fig 1 shows the percentage of Carbon & Nitrogen & CN Ratio in components of MSW in Bhopal.

III. CASE STUDY

| 1 | able 5 Carbo | n muogen rat | 10 |
|---------------|--------------|--------------|----------------|
| Material | Carbon | Nitrogen | Carbon |
| | % | % | Nitrogen Ratio |
| Soyabean | 41 | 1.30 | 32/1 |
| Peanut leaves | 11 | 0.59 | 19/1 |
| Corn | 40 | 0.75 | 53/1 |
| Rice | 42 | 0.53 | 67/1 |
| Wheat | 46 | 0.53 | 87/1 |
| Leaves | 41 | 1 | 41/1 |
| Animal dung | 7.3 | 0.60 | 13/1 |

Table 3 Carbon nitrogen ratio

Observations and findings based over primary study:

The usual practice among restaurant owners and workers to calculate frequency of waste generation in different days. Some of owners dumped wastes besides the road as usual and some of them to municipal container. However, almost all owners had to dispose of some of the fruits and vegetables at the end of the day as they become rotten.

Food waste analysis:



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Meals, juice, braveries, meat, leaves and rotten fruits, eggs and vegetables are the main types of waste. There were different opinions regarding which season generated highest amount of food vegetable waste. Few were who serve fruit juice have different opinion that in rainy season, waste was highest as it is difficult to store the fruits and vegetables for a longer duration and during summer, it was least as less fruits and vegetables were available in the market. This waste is then collected by the corporation workers the next day morning.

Among the Six restaurants which were visited, one restaurant generated approximately 200 kg of food waste per day and also practiced segregation of food and non-food waste. Food waste mainly comprised of rotten food and vegetable peels and was found to be highest during summer season. After segregation, they disposed the waste in corporation bins which would be collected by workers. Another restaurant was found to dispose the waste without segregation. One restaurant claimed to generate waste of insignificant quantity to the tune of 5 to 7 kg per day. Data on quantity of food waste was not maintained in DB mall and it was found that waste was not segregated. As food is served in portions in most of the restaurants inside DB mall, the food wastage was minimal comprising of approximately 10% of the total waste in food court which was mainly comprised of disposables such as plates, spoons, etc.

Testing for samples:

The raw municipal solid waste (MSW) and food waste was collected from the MP Nagar Zone 1 area. It occupies an area of approx 1 acre. It receives approximately 1500 kg of food waste along with municipal solid waste per day which containing about 80-90% of organic waste. The sample was collected, delivered to the laboratory at Indian institute of agriculture science and Indian institute of forest management. The techniques used for sampling analyses were in accordance with the Standard Method for the Examination of waste. The compositions of the feed sample are summarized in Table

| S.no. | Elements | Digester I | Digester 2 |
|-------|----------|------------|------------|
| 1 | pН | 4.39 | ≤7.2 |
| 2 | BOD | 13981 | 300 |
| 3 | COD | 20087 | 2575 |
| 4 | TS | 1058 | 672 |
| 5 | TSS | 410 | <10 |

Table 4 CHARACTERISTICS OF THE PREPAIRED FEED S

Study based over Experimental conditions:

For primary design criteria was based to the study of different Biogas yields because everyone has own and different COD concentration at maintained pH and also studied to removal of pollutants. In this study, the batch reactors were filled with fresh prepared slurry feed. The digesters were dozed with N2:CO2-80:20 for5 min to minimize air contamination, air tight, and subsequently maintained at 35°C for next 20 days. The digester was maintained in anaerobic conditions and it was allowed to stabilize for one week. During this stabilization period, digester temperature of 26 to 36°C was monitored and pH was maintained in the range of 6.5 to 7.5 by adding sodium hydroxide and COD, TSS and VSS reduction were also monitored. Steady-state condition was identified when the COD value of the effluent and the daily biogas production were measured to be the same for two or three consecutive days. A magnetic stirrer was introduced for vigorous mixing. Each experiment was performed in duplicate to determine experimental benefits and error to improve design.

| Ta | able 5 Avera | ge production rate | e of biogas | in differe | nt digester |
|----|--------------|--------------------|-------------|------------|-------------|
| S | Biogas | Methane | COD | COD | Туре |
| no | Production | Yield | Initial | Final | |
| | | | | | n · |

 no
 Production
 Field
 Initial
 Final

 1
 1.8±1.3
 .002±0.0100
 21050
 7250
 Digester1

 2
 0.6±0.5
 0.190±0.020
 3204
 540
 Digester2

All data provided by the lab where we tested our food waste sample for methane generation with following this process.

At the practical level food waste after separation from MSW, a feed was prepared and in the plant of 2000 kg from day one to next 20-30 days, feed (food waste) 10-100 kg at various days. Every evening collected waste from MP



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Nagar area was filled to the chamber and after 24 hour % increase in methane and % of slurry were measured with installed gage mounted over plant in supervision of plant team and me as a visitor.

| able 6 Firs | st biogas plant stu | dy for methane gen |
|-------------|----------------------------|--------------------|
| S no | Feed/day | % methane |
| 1 | 10kg/1 st day | 0-0.5% |
| 2 | 20kg/2 nd day | 0-0.8% |
| 3 | 20kg/3 rd day | 0.08% |
| 4 | 20kg/4 th day | 0.08-0.09% |
| 5 | 30kg/5 th day | 0.08-0.09% |
| 6 | 50kg/10 th day | 2.04-2.06% |
| 7 | 50kg/11 th day | 2.04-2.06% |
| 8 | 50kg/15 th day | 2.04-2.06% |
| 9 | 75kg/16 th day | 3.08-4.01% |
| 10 | 100kg/20 th day | 4.02-4.057% |

Table 6 First biogas plant study for methane generation

| | ady for methane g |
|----------------------------|---|
| Feed/day | % Methane |
| 10kg/1st day | 0-0.2% |
| 20kg/2nd day | 0-0.6% |
| 20kg/3rd day | 0.07% |
| 20kg/4th day | 0.07-0.09% |
| 30kg/5th day | 0.07-0.09% |
| 50kg/10th day | 1.841.92% |
| 50kg/11th day | 1.52-1.8% |
| 50kg/15th day | 1.92-2.04% |
| 75kg/16th day | 2.04-3.25% |
| 100kg/20 th day | 3.20-3.44% |
| | 10kg/1st day 20kg/2nd day 20kg/3rd day 20kg/4th day 30kg/5th day 50kg/10th day 50kg/11th day 50kg/15th day |

After comparing both working plant after feeding food waste in different quantity on various days, result was more than expected. And this may be because of unutilized contain and vitamins or starch available in waste which increased the production rate of methane in same plant.

Observations were based over two different plants at two different climate and geographical location, first observation from a plant situated to agriculture land and second one was at hilly area, and we can see the difference between these two.

As we know at hill top there is some maintained humidity which affected production rate and the first one situated over agriculture land having best atmosphere support because of maintained temperature and stream flow of wind and less humidity factor.

Calculation

Energy available in 1m³ plant at end of the month: We know that Biogas contains 60% (approx and known value) Methane.

Calorific Value of methane = 58 MJ/kg (approx and known value)

Density of Methane at NTP = 0.668 kg/m^3 (approx and known value)

Therefore, Calorific value of methane = $58 \times 0.668 = 38.74 \text{ MJ/m3}$

In biogas generation only methane can be used as fuel so;

Calorific value of Biogas = $0.6 \times 38.74 \text{ MJ/m3} = 23.24 \text{ MJ/m3}$

If a plant of 1 m³ capacity produces 0.8 m³ of gas per day.

Total energy in 0.8 m^3 of biogas = 18.59 MJ

Total energy in 0.8 m^3 of biogas = 0.8 x 23.24 MJ



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Assuming that the efficiency of a biogas stove and LPG stove is the same Energy provided per month = 18.59 x 30 Energy provided per month = 557.76 MJ Therefore a biogas plant of 1 m³ capacity is equivalent to 75-80 % of an LPG cylinder per month. Feasibility study for implementing the project in M.P Nagar Bhopal: Bhopal M P Nagar restaurants meals for many customers & food is prepared as well. If customers hus al

Bhopal, M.P Nagar restaurants meals for many customers & food is prepared as well. If customers buys about 4 cylinders per month which are used only for preparing the one time meal for them or their family as well.

Then, 4 cylinders of LPG = $4 \times 738.4 \text{ MJ} = 2953.6 \text{ MJ}$

4 cylinders of LPG = 4 x /38.4 MJ = 2953.6 MJ

Energy required per day = 2953.6/24 MJ = 123.06 MJ

Energy obtained per cubic Meter of biogas = 23.24 MJ

Gas requirement to supplement 50% of gas use = $123.06 \times 0.5/23.24 \text{ m}^3 = 2.64 \text{ m}^3$

Therefore required size of digester = $2.64/0.7 \text{ m}^3 = 3.77 \text{ m}^3$ (calculation done with approx values) Therefore 4 m³ digester and 3 m³ gas collector should provide 60% of the energy requirements.

IV. RESULT

During feed of slurry at different digester was maintained 35°C to achieve maximum methane production. To maintain that temperature for slurry and gas holding vessel it was necessary to maintain constant temperature, for that this data has been developed via MATLAB to calculate need of heat supply at slurry

Result of Computations of Heat Losses when Slurry is at 20°C

 $\begin{array}{l} Q = [h \ 1 \ At \ (TD - T \ A) + h3 \ At \ (TD - TG)] \\ Slurry \ Cooling \ Heat \ Loss: \ Q = m \times Cp \times (T2 - T1) \\ Slurry \ to \ Ground \ Heat \ Loss: \ Q = h6 \ AW \ (TS - T\infty) \end{array}$

| Table 8 Heat Loss Due to Radiation | | |
|------------------------------------|-----------------------------|---------------------|
| Time | Heat loss via Heat loss via | |
| (hours) | Radiation from top | Radiation from wall |
| 1 | 139.7 | -17.89 |
| 2 | 140.1 | -17.98 |
| 3 | 148.8 | -22.9 |
| 4 | 110.7 | -27.2 |
| 5 | 26.24 | -81.5 |
| 6 | 18 | -248.5 |
| 7 | 93.7 | -652.8 |
| 8 | 189.13 | -507.8 |
| 9 | 185 | -278.61 |
| 10 | 375.89 | 12 |
| 11 | 564.12 | 793 |
| 12 | 745.78 | 1287.56 |
| 13 | 889.71 | 1802.8 |
| 14 | 870.37 | 1674.2 |
| 15 | 877.32 | 3589.78 |
| 16 | 557.89 | 4547.65 |
| 17 | 598.78 | 798.59 |
| 18 | 571 | 802.5 |
| 19 | 428.75 | 485.56 |
| 20 | 345.78 | 409.74 |
| 21 | 267 | 202.89 |
| 22 | 196.75 | 107.87 |
| 23 | 207.32 | 109.27 |
| 24 | 98.78 | -19.81 |



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| Table 9 Heat Loss Due to Convection | | |
|-------------------------------------|---------------------|---------------------|
| Time | Heat loss from | Heat loss from |
| (hours) | roof via convection | wall via convection |
| 1 | 115.56 | -312.32 |
| 2 | 139.05 | -482.98 |
| 3 | 155.2 | -355.78 |
| 4 | -48.62 | -790.31 |
| 5 | 169.45 | -698.15 |
| 6 | 205.4 | -425.46 |
| 7 | 382.15 | 16.9 |
| 8 | 685.26 | 1389.1 |
| 9 | 1089.41 | 2489.26 |
| 10 | 1537.29 | 3689.5 |
| 11 | 1739.8 | 4287.66 |
| 12 | 1632.5 | 4456.32 |
| 13 | 1438.91 | 3789.16 |
| 14 | 1381.84 | 785.92 |
| 15 | 896.7 | 2238.35 |
| 16 | 759.32 | 2938.25 |
| 17 | -42.89 | 1492.89 |
| 18 | -56.41 | 548.63 |
| 19 | 283.72 | 452.36 |
| 20 | 201.25 | 394.2 |
| 21 | -16.89 | -12.1 |
| 22 | 87.82 | 165 |
| 23 | 182.39 | -190.1 |
| 24 | 138.88 | -301.75 |

V. CONCLUSION

Using food waste as a feed from a located area of MP Nagar to harness biogas at certain temperature of 35°C will be optimal. This is because optimum temperature for the anaerobic fermentation lies within the narrow limits (30°C-35°C). As well the gas holder temperature were calculate, experimentally and via programming when slurry is maintained at 20°C. Result shows computational value matches with experimental value, and selected value of heat transfer co-efficient represent real system. Again, gas holder temperature calculated at program when slurry is at 35°C.Heat loss from the biogas plant has calculated at 20°C & 35°C, and then the relational table has been created based on the value and also graphical representation were generated. Energy required to charge daily kitchen waste from 20°C to 35°C has considered. For external heat supply a solar water heater system with auxiliary heater is designed. Experimental results in the month of January shows, average generated gas is 120.9 m³/day only (rated 85-100 m³/day), this is because of plant is not maintaining optimum temperature for anaerobic fermentation and average feeding is 1200kg/day instead of 2000 kg/day. In conclusion, the result of thermal analysis is used to define a strategy for operating biogas plant at optimum temperatures

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